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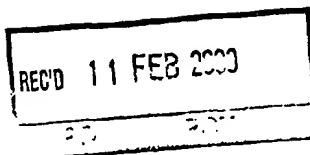


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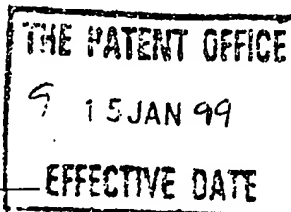
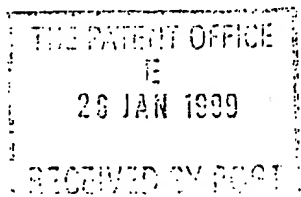
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9

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Request for grant of a Patent Form 1/77

15 JAN 1999

Patents Act 1977

1 Title of invention

1 Please give the title of the invention

9900836-9
IMPROVEMENTS IN AND RELATING
TO PROCESSING MATERIALS

2 Applicant's details

☐ First or only applicant

2a If you are applying as a corporate body please give:

Corporate name

BRITISH NUCLEAR FUELS PLC

Country (and State of incorporation, if appropriate)

UNITED KINGDOM

2b If you are applying as an individual or one of a partnership please give in full:

Surname

Forenames

2c In all cases, please give the following details:

Address

RISLEY
WARRINGTON
CHESHIRE

UK postcode WA3 6AS
(if applicable)

Country UNITED KINGDOM

ADP number
(if known)

350108001

2d, 2e and 2f:
If there are further applicants
please provide details on a separate
sheet of paper.

☐ **Second applicant (if any)**

2d If you are applying as a corporate body please give:

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Country (and State of incorporation, if appropriate)

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Forenames

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3
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3 Address for service details

3a Have you appointed an agent to deal with your application?

Yes ☒ No ☐ ➔ go to 3b

↓
Please give details below

Agent's name

URQUHART-DYKES & LORD

Agent's address

TOWER HOUSE

MERRION WAY

LEEDS

Postcode LS2 8PA

Agent's ADP number 1644004

3b:
If you have appointed an agent,
all correspondence concerning
your application will be sent to
the agent's United Kingdom
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3b If you have not appointed an agent please give a name and address in the United Kingdom to which all correspondence will be sent:

Name

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Postcode
ADP number
(if known)

Daytime telephone
number (if available)

4 Reference number

4 Agent's or applicant's
reference number
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ANP/P17562

5 Claiming an earlier application date

5 Are you claiming that this application be treated as having been filed on the date of filing of an earlier application?

Yes ☐ No ☒ **go to 6**

↓
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☐ number of earlier
application or patent
number

☐ filing date
(day month year)

☐ and the Section of the Patents Act 1977 under which you are claiming:

15(4) (Divisional) ☐ 8(3) ☐ 12(6) ☐ 37(4) ☐

6 Declaration of priority

6 If you are declaring priority from previous application(s), please give:

Country of filing	Priority application number (if known)	Filing date (day, month, year)
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6

If you are declaring priority from a PCT Application please enter 'PCT' as the country and enter the country code (for example, GB) as part of the application number.

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7

The answer must be 'No' if:

- any applicant is not an inventor
- there is an inventor who is not an applicant, or
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8

Please supply duplicates of claim(s), abstract, description and drawing(s).

Please mark correct box(es)

9

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7 Inventorship

7 Are you (the applicant or applicants) the sole inventor or the joint inventors?

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A statement of Inventorship on Patents Form 7/77 will need to be filed (see Rule 15).

8 Checklist

8a Please fill in the number of sheets for each of the following types of document contained in this application.

Continuation sheets for this Patents Form 1/77

Claim(s)

Description

Abstract

Drawing(s)

8b Which of the following documents also accompanies the application?

Priority documents (please state how many)

Translation(s) of Priority documents (please state how many)

Patents Form 7/77 - Statement of Inventorship and Right to Grant (please state how many)

Patents Form 9/77 - Preliminary Examination/Search

Patents Form 10/77 - Request for Substantive Examination

9 Request

I/We request the grant of a patent on the basis of this application.

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Date

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IMPROVEMENTS IN AND RELATING TO PROCESSING MATERIALS

This invention concerns improvements in and relating to processing of materials, particularly, but not exclusively to the processing of nuclear fuel materials, materials involved in the nuclear fuel cycle and materials involved in the nuclear fuel industry.

The production of fuel grade nuclear fuel is a long and complicated process. For instance, starting from mined uranium ore, in general terms the process involves taking the ex-mine grade material and gradually converting and enriching it until it is in a form and of a grade suitable for the production of fuel pellets.

Prior art systems for converting the ore into material suitable for enrichment, by physical or chemical means, have almost invariably involved a series of wet chemical techniques. For instance, the initial uranium oxide is concentrated in a uranyl nitrate hexahydrate based stage; with a de-nitration stage to convert the material into UO_3 ; this is then reduced to convert the UO_3 to UO_2 ; with a hydro-fluorination stage to form UF_4 and further fluorination subsequently UF_6 , which is fed to the enrichment procedures use.

Similar complex chemical and physical steps, generally involving wet chemistry, are used in the recycling of spent fuel and other uranium containing feeds.

The present invention aims to provide an alternative route for converting a variety of uranium and other nuclear material containing feeds into a variety of products, including fuel grade materials.

According to a first aspect of the invention we provide a process for treating a uranium containing feed material, the process comprising :-

contacting the uranium containing material with fluorine gas, the fluorine reacting with the uranium containing material to give uranium fluoride;

feeding the uranium fluoride to a separator stage, the separator stage converting the uranium fluoride into a plasma and/or ionised ^{form} at least part of the uranium being ionised and at least part of the fluorine being non-ionised, the ionised parts being contained in a magnetic field to form a first product stream, the non-ionised parts being withdrawn from the magnetic field to form a second product stream;

the second product stream being recycled to the fluorine gas and uranium containing material contact stage.

The uranium containing feed material may be a uranium ore. The ore may be ex-mined and/or higher uranium content.

The uranium containing feed material may be uranium and/or uranium oxide from the reprocessing of uranium and/or uranium containing material previously used in the nuclear fuel cycle.

The uranium containing feed material may be uranium containing residues from one or more processes, for instance enrichment process streams, including waste or by-product streams thereof.

The uranium containing feed material may be spent fuel from a nuclear reactor. The spent fuel may contain fission products and/or plutonium isotopes, as well as uranium.

One or more of the above mentioned feed types may be fed to the process simultaneously.

The uranium fluoride produced may be mixed fluoride forms, but preferably the predominant uranium fluoride is uranium hexafluoride.

A material removal stage may be provided prior to the separator stage. Uranium fluoride, particularly uranium hexafluoride may be removed from the process at this stage. The uranium fluoride may be fed to an enrichment process and/or be stored and/or transported to a remote location and/or sold. Impurities may be removed from the process, particularly where the uranium containing feed material is uranium ore, at this stage. The impurities may be removed as fluorinated impurities.

The separator stage may be provided according to the details provided below.

The first product stream may comprise uranium metal. The uranium metal may be used to produce MAGNOX fuel. The uranium metal may be fed to a subsequent process, for instance an enrichment process. The enrichment process may be an AVLIS and/or ~~OTHER METAL BASED~~ enrichment process. The enrichment process may be provided according to the details provided below. The first product stream, particularly where a spent fuel feed is involved, may comprise uranium and/or plutonium and/or fission products in elemental form. The elemental ~~form~~ may be used as a storeable form of the spent fuel material.

The second product stream is preferably predominantly fluorine. The fluorine may be in atomic form, but is preferably allowed to return to molecular form, F_2 .

The second product stream may be processed prior to feeding to the fluorine/uranium containing material contact stage. The process may comprise cleaning the fluorine to remove other species.

The level and/or amount of fluorine in the second product stream may be increased prior to feeding to the fluorine/uranium containing material contact stage from an external source. The external source may be provided according to the third aspect of the invention.

According to a second aspect of the invention we provide apparatus for treating a uranium containing feed material, the apparatus comprising :-

a first unit in which the uranium containing material is contacted with fluorine gas, the fluorine reacting with the uranium containing material to give uranium fluoride;

a second unit forming a separator stage to which the uranium fluoride is fed, the separator stage including a plasma and/or ion generator to convert the uranium fluoride into a plasma and/or ionised, at least part of the uranium being ionised and at least part of the fluorine being non-ionised, the separator stage further including magnetic field generating means to form a magnetic field to contain the ionised parts and form a first product stream, the separator stage still further including means for removing non-ionised parts from the magnetic field, the non-ionised parts being withdrawn from the magnetic field to form a second product stream;

the second product stream being recycled to the first unit in which the fluorine gas and uranium containing material are contacted.

According to a third aspect of the invention we provide a process for fluorinating a uranium containing feed material, the method comprising:

contacting the uranium containing material with fluorine gas, the fluorine reacting with the uranium containing material to give uranium fluoride;

the fluorine gas being produced by feeding a fluorine containing material to a separator stage, the separator stage

converting the fluorine containing material into a plasma and/or ionised form, at least part of the non-fluorine part of the feed being ionised and at least part of the fluorine part of the feed being non-ionised, the ionised parts being contained in a magnetic field to form a first product stream, the non-ionised parts being withdrawn from the magnetic field to form a second product stream;

the second product stream being fed to the fluorine gas and uranium containing material contact stage.

The uranium containing feed material may be provided as defined in the first aspect of the invention. The uranium fluorides produced may be as defined in the first aspect of the invention.

The fluorine containing material may be a material from the nuclear fuel production process. Preferably the fluorine containing material is a uranium fluoride, and more preferably uranium hexafluoride. Ideally the uranium fluoride is depleted in ^{235}U , and is still more preferably UF_6 which is depleted in ^{235}U . The UF_6 may be a feed from another process and/or another part of the same process and/or a feed from a stored source of UF_6 .

The first product stream preferably contains uranium, and in particular depleted uranium. The first product stream may be used as a storeable form of depleted uranium.

Preferably the second product stream supplements fluorine being recycled from a separator according to the process of the first aspect of the invention.

According to a fourth aspect of the invention we provide apparatus for fluorinating a uranium containing feed material, the apparatus comprising:

a first unit in which the uranium containing material is contacted with fluorine gas, the fluorine reacting with the uranium containing material to give uranium fluoride;

a second unit forming a separator stage, the fluorine gas being produced in the separator stage by feeding a fluorine containing material to the separator stage, the separator stage including a plasma and/or ion generator to convert the fluorine containing material into a plasma and/or ionised form, at least part of the non-fluorine part of the feed being ionised and at least part of the fluorine part of the feed being non-ionised, the separator stage further including magnetic field generating means, the ionised parts being contained in a magnetic field produced by the magnetic field generating means, to form a first product stream, the separator stage still further including means to remove non-ionised part from the magnetic field, the non-ionised parts being withdrawn from the magnetic field to form a second product stream;

the second product stream being fed to the first unit in which fluorine gas and uranium containing material are contacted.

According to a fifth aspect of the invention we provide a process for enriching a uranium containing feed material, the process comprising :

introducing the uranium containing material to a separator stage, the separator stage converting the uranium containing material into a plasma and/or ionised form, at least part of the uranium being ionised and at least part of the non-uranium part of the feed being non-ionised, the ionised parts being contained in a magnetic field to form a first product stream, the non-ionised parts being withdrawn from the magnetic field to form a second product stream;

the first product stream being fed to an enrichment stage, the enrichment stage applying one or more frequencies of electromagnetic radiation to the first product stream, the one or more frequencies being chosen to selectively ionise one or more components of the first product stream, the selectively ionised

components being separated from the selectively non-ionised components to form third and fourth product streams respectfully.

The uranium containing feed material may be provided according to the feed materials of the first aspect of the invention, but it is preferred that the uranium containing feed material be one or more uranium fluorides and in particular uranium hexafluoride.

The separator may be provided as detailed below.

Preferably the first product stream predominantly contains the uranium of the feed material. Preferably the second product stream predominantly contains the non-uranium part of the feed material and particularly the lower atomic mass components.

The first product stream, and particularly the uranium therein, may be feed to the enrichment stage in still ionised form.

Preferably, however, the first product stream, and particularly the uranium therein, and still more particularly the ^{235}U therein, is neutralised prior to the enrichment stage. The first product stream, and particularly the uranium therein, is preferably fed to the enrichment stage in gaseous and/or vapour form.

Preferably the one or more frequencies of electromagnetic radiation applied are selected to ionise the ^{235}U containing components in preference to the ^{238}U containing components.

The components may be molecules, such as UF_6 , incorporating the respective isotopes of uranium, but are preferably the atomic form of the isotopes themselves.

The third product stream may be separated from the fourth product stream by electrostatically attracting the third product stream to a collection location. The fourth product stream is preferably collected at a separate location.

Preferably the third product stream is enhanced in one or more isotopes, ideally ^{235}U , relative to the first product stream. Preferably the fourth product stream is depleted in the said one or more isotopes, ideally ^{235}U , relative to the first product stream.

The third and/or fourth product streams may be subject to further processing.

According to a sixth aspect of the invention we provide apparatus for enriching a uranium containing feed material, the apparatus comprising :

a first unit, forming a separator stage, into which the uranium containing material is introduced, the separator stage including a plasma and/or ion generator to convert the uranium containing material into a plasma and/or ionised form, at least part of the uranium being ionised and at least part of the non-uranium part of the feed being non-ionised, the separator stage further including magnetic field generating means for producing a magnetic field, the ionised parts being contained in the magnetic field to form a first product stream, the separator stage still further including means to remove non-ionised parts from the magnetic field, the non-ionised parts being withdrawn from the magnetic field to form a second product stream;

a second unit, forming an enrichment stage to which the first product stream is fed, the enrichment stage including a source of electromagnetic radiation, preferably a laser, so as to apply one or more frequencies of electromagnetic radiation to the first product stream, the one or more frequencies being chosen to selectively ionise one or more components of the first product stream, the enrichment stage further including means to separate the selectively ionised components from the selectively non-ionised components to form third and fourth product streams respectively.

According to a seventh aspect of the invention we provide a process for purifying a uranium containing material, the process comprising:

feeding a uranium containing material to an enrichment stage, the enrichment stage applying one or more frequencies of electromagnetic radiation to the feed thereto, the one or more

frequencies being chosen to selectively ionise one or more components of the feed thereto, the selectively ionised components being separated from the selectively non-ionised components to form third and fourth product streams respectfully;

one or both of the product streams being fed to a fluorinating stage in which the uranium containing material in the product stream is contacted with fluorine gas, the fluorine reacting with the uranium containing material to give uranium fluoride;

the fluorinated uranium and other components of the product stream being fed to a separation stage in which the uranium fluoride is separated, to give a fifth product stream, from one or more other components of the product stream which forms a sixth product stream.

Preferably the uranium containing material fed to the enrichment stage is atomic uranium, preferably in gaseous and/or vapour form, preferably in non-ionised form.

Preferably the enrichment stage enriches the material fed to it in the manner of the fifth aspect of the invention detailed above.

The fourth product stream may be fed to the fluorinating stage, but it is particularly preferred that the third product stream is so fed.

Preferably the uranium fluoride produced is as detailed in the first aspect of the invention above.

The other components of the product stream may be one or more other metals, and in particular may be iron. Preferably the iron is also fluorinated in the fluorination stage.

The uranium fluoride may be separated from the one or more impurities, preferably also in fluoride form, based on differences in volatility, and most preferably the higher volatility of the uranium fluoride, ideally uranium hexafluoride. The fifth and/or sixth product streams may be subjected to further processing.

According to a further aspect of the invention we provide apparatus for purifying a uranium containing material, the apparatus comprising:

a first unit forming an enrichment stage to which a uranium containing material is fed, the enrichment stage including a source of electromagnetic radiation, preferably a laser, to apply one or more frequencies of electromagnetic radiation to the feed thereto, the one or more frequencies being chosen to selectively ionise one or more components of the feed thereto, the enrichment stage further including means to separate the selectively ionised components from the selectively non-ionised components to form third and fourth product streams respectively;

a second unit forming a fluorinating stage, to which one or both of the product streams are fed in which the uranium containing material in the product stream is contacted with fluorine gas, the fluorine reacting with the uranium containing material to give uranium fluoride;

a third unit forming a separation stage, the fluorinated uranium and other components of the product stream being fed to the separation stage in which the uranium fluoride is separated, to give a fifth product stream, from one or more other components of the product stream which forms a sixth product stream.

The various aspects of the invention detailed above may be combined with one another. For example the fluorine production process of the third aspect of the invention may be used to contribute to the fluorine requirements of the fluorinating stage of the first aspect of the invention. Similarly the fluorine production process of the third aspect of the invention may be used to contribute to the fluorine requirements of the fluorinating stage of the seventh aspect of the invention. It is also possible for the separator of the first aspect of the invention and the fifth aspect of the invention to be one and the same, with the

first product stream from the separator going to the enrichment stage. This combined process could also use the third aspect of the invention to contribute to its fluorine requirements in the fluorinating stage. Additionally it is also possible, with or without the separator of the first aspect as the separator of the fifth aspect too, for the enrichment stage of the fifth aspect to be one and the same as the enrichment stage of the seventh aspect of the invention. The first, third, fifth and seventh aspects of the invention may all form a single process.

The feed may be introduced to the magnetic field as a gas, liquid, solid or mixture of states. A gas feed to the magnetic field is preferred.

The feed may be introduced to the plasma generation means as a gas, liquid, solid or mixture of states.

The feed may be introduced to the ionisation means as a gas, liquid, solid or mixture of states. A gas feed to the ionisation means is preferred, particularly where a plasma generator is not also provided.

The feed may be provided in gaseous form by boiling and/or evaporation and/or sublimation of a solid or liquid initial feed. The conversion to gaseous state may be effected by a furnace, microwave heater or other form of heater means. Preferably the gas is introduced prior to ionisation

Preferably all, or substantially all, of a given component is ionised. Preferably all, or substantially all, of a given component is not ionised.

Preferably some or all metallic elements present in said feed are ionised. The ionisation of metallic elements with an atomic weight greater than 90 is particularly preferred. Preferably some or all non-metallic elements in said feed are not ionised. Preferably all elements with an atomic weight below 90, most preferably below 70 and ideally below 60, are left in non-ionised form. It is particularly preferred that elements such as uranium and/or plutonium and/or thorium and/or gadolinium are ionised. It is preferred that elements such as hydrogen and/or fluorine and/or oxygen and/or nitrogen are not ionised. Preferably boron is not ionised. Preferably

The ionisation of the components may be caused by the temperature of the plasma. Additionally or alternatively the ionisation of the components may be caused by the interaction of the components with high energy electrons produced by electron cyclotron resonance.

The extent of ionisation and/or components ionised may be controlled by the energy input of and/or residence time in the electron cyclotron resonance unit.

Preferably the ionisation is controlled by the level of energy input. The level of energy input may be controlled by controlling the temperature of the plasma. Preferably the energy input is not selective between components of the feed. In this way all of the components of the feed are preferably raised to the same energy level. Preferably the ionised and non-ionised feed components are in equilibrium with one another for the prevailing conditions.

The feed material may be converted to a gas and fed to an ECR unit for ionisation. A furnace heater or evaporator may be used to convert the solid or liquid feed to gaseous / vapour form.

In a particular embodiment, therefore, the plasma may convert the feed materials to discrete atoms and electron cyclotron resonance may subsequently give rise to at least partial ionisation, preferably of a selective nature.

Preferably the feed is provided in molecular form and selectively separated as discrete atoms and/or elemental forms from ionised discrete atomic forms and/or elemental forms. This renders the technique applicable to a wider variety of materials than are possible with elemental feed and separation in elemental form or molecular feed followed by separation in molecular form.

The temperature of said plasma may be controlled to provide selective ionisation of the components in the desired way. Thus the plasma may ionise some components in the feed but leave other components, such as fission products and/or non-metallic elements, un-ionised.

Preferably said plasma is provided at 3000 to 4500K. Preferably said plasma is generated by microwave or radio frequency means. Preferably the plasma in the generator is operated at between 1000 and 10000 Pa. A value of 2000 +/- 10% is preferred.

Additionally or alternatively the residence time of the feed within the plasma prior to the separation may be controlled to provide selective ionisation of the components in the desired way.

Preferably the feed is introduced into the containing magnetic field in un-ionised form. Preferably the partial ionisation process occurs within the magnetic field on an uncharged gas. The gas may be in molecular and/or atomic form.

The magnetic field may be configured to define a cylindrical active volume in which the plasma/ions are processed. Preferably the plasma/ions pass along the axis of this containment area from the plasma generation and/or ionisation means to the next, separation, stage.

Preferably the separation of ionised and un-ionised components is affected by removing the un-ionised component from the plasma, most preferably as a gas. The un-ionised components may be pumped away from the ionised component. The ionised component is contained and hence restrained by the magnetic field.

The separation of ionised from non-ionised components may be effected in a number of stages. Preferably the stages are discrete from one another. The stages maybe separated from one another by a baffle provided with an aperture. Preferably the aperture is entirely within the containment area of the magnetic field. Preferably one or more of the stages are operated at different pressures to one or more other stages. The pressure level may be maintained by the pumping level employed. Preferably the pressure in one or more stages near to the inlet is higher than one or more further away from the inlet. Preferably the pressure decreases for each zone relative to the preceding stage nearer the inlet. Preferably the pressure in each stage is 30% to 60% of that in the preceding stage, progressing away from the inlet.

Preferably three stages are provided. Each stage may be between 0.5 and 2m in length.

Preferably the first stage is operated at between 10 and 50 Pa. A level of 40 Pa \pm 10% is preferred.

Preferably the second stage is operated at between 5 and 20 Pa. A level of 16 Pa \pm 10% is preferred.

Preferably the third stage is operated at between 2 and 10 Pa. A level of 7 Pa \pm 10% is preferred.

The separated un-charged components may be recycled for subsequent use and/or subjected to further processing. This may include further selective ionisation and / or selective processing to separate different components.

The separated charged components are preferably still contained in a magnetic field. The separated charged components may be subjected to further processing including selective de-ionising; de-ionising followed by further selective ionisation; or other selective processing to separate different components.

The enrichment stage referred to in the above mentioned aspects may have one or more of the following features.

The enrichment stage may be evacuated, for instance to 10^{-6} torr or less.

The electromagnetic radiation may be applied by one or more laser beams and/or one or more lasers. Preferably the selective ionisation generated is photoionisation. Ionisation and/or excitation may occur in one or more stages, preferably with different frequencies selected for different stages.

The separation of ionised and non-ionised components may be effected by electrostatic attraction of the ionised species to a collection location, such as one or more collection plates. More preferably the ionised and non-ionised components are separated by deflecting the ionised components using a magnetic field.

Various embodiments of the invention will now be described, by way of example only, and with reference to the accompanying drawings in which:-

Figure 1 illustrates a first embodiment of the invention for producing purified uranium containing materials;

Figure 2 illustrates a modification to the process of Figure 1 for introducing fluorine to the circuit;

Figure 3 illustrates a modified circuit for processing spent fuel materials;

Figure 4 illustrates a further embodiment of the invention;

Figure 5 illustrates one embodiment of a separator stage suitable for use in the process routes of the invention;

Figure 6 illustrates an alternative embodiment of a separator suitable for use in the process routes of the invention; and

Figure 7 illustrates an enricher suitable for use in the process routes of the present invention.

Figure 1 illustrates a direct fluorination stage 2 in which the metallic components of interest are fluorinated followed by a fluorine / metal separation stage 4 to give rise to a variety of potential product forms and fluorine which is recycled through stage 6 back to the direct fluorination stage. This system can be used for a variety of potential feeds with a variety of intended product forms.

Uranium Ore Concentrate Feed

The process offers the potential for feeding uranium ore concentrate from stage 8 into the direct fluorination stage 2 where the uranium oxide is converted to uranium

fluoride, principally UF_6 , by the introduction of fluorine. The UF_6 then passes to a cleaning stage 10 at which point a variety of impurities present in the ore concentrate can be removed, in various forms, again including principally fluorinated forms. These form waste stream 12. It is also possible at this stage to tap from the process UF_6 for sale or use in other processes, product stream 14.

As part of the intended process, however, a substantial portion of UF_6 continues from cleaning stage 10 to separation stage 4. In the separation stage 4, which is discussed in more detail below, the uranium and other metal species are separated from the fluorine and other low atomic weight materials. The fluorine returns as stream 16 to stage 6 for subsequent feed back to the direct fluorination stage 2. The level of fluorine in the system can be topped up from a fluorine source 18 which feeds to stage 6 also.

It is a major advantage of the present technique that the expensive fluorine is used for the separation of uranium from other impurities in the ore, but that the fluorine is recovered and recycled back to the fluorination stage 2 for subsequent re-use. A substantially closed circuit with regard to the fluorine is thus provided.

The metallic product stream from stage 4 may form product stream 20 to subsequent processing, discussed in more detail below, or alternatively may form a uranium metal product stream 22, for instance for use as a magnox fuel.

Re-processed Uranium Feed

The system outlined above with reference to Figure 1, can equally well be used with a feed from stage 24 consisting of re-processed uranium, predominantly UO_2 . The re-processed uranium is obtained from a variety of potential sources, including uranium extracted from spent fuel rods.

Once again, the uranium oxide is fed to a direct fluorination stage for conversion to UF_6 . Once again, it

will be possible to remove a product stream 14 consisting of UF_6 , the uranium being re-processed uranium.

The impurity removing stage 10 may or may not be necessary for re-processed uranium feed.

Once again, in separation stage 4 the uranium is split from the fluorine with the fluorine being recycled. The uranium then either passes to further processing, for instance to enrich it, or alternatively is used for the production of magnox fuel.

Uranic Residue Feeds

A variety of existing processes linked to the production of uranium fuels produce residue streams which require processing. These streams generally consist of uranium in oxide form and as a consequence, such streams 26 are adapted to feeding to the fluorination stage 2 in the process outlined above. Once again, the uranium can be extracted for subsequent further processing as desired.

Fluorine Replenishment Route

Particularly with regard to the processing of uranium ore concentrates, where fluorinated impurities are removed from the process in stage 10, it is necessary to add fluorine to the circuit to replace the fluorine which is lost with these impurities. The fluorine can come from a variety of sources, but a preferred production route is outlined in Figure 2.

Figure 2 illustrates the fluorine source stage 6 to which fluorine is fed from the separation stage as stream 16 and is fed back to the fluorination stage 2. The top up fluorine is introduced into this stage 6 from stream 28.

The feed stage 30 for this part of the process provides a source of UF_6 and it is particularly preferred that this be the depleted stream of UF_6 arising from the enrichment part of the process itself, detailed below, or alternatively from

the existing enrichment techniques and / or stockpiles of depleted UF_6 historically produced. Depleted UF_6 generally consists predominantly of $^{238}\text{UF}_6$ from which the vast majority of $^{235}\text{UF}_6$ has been removed in enrichment processes.

The UF_6 feed from stage 30 is fed to separation stage 32, which is preferably of a similar type to the separation stage 4 outlined above in Figure 1, and discussed below in more detail.

The separation stage 32 produces the desired stream of fluorine, 28, to feed into the fluorine circuit and separate product stream 34. Preferably the product stream 34 is uranium metal which is a more suitable form for long term storage than UF_6 . This is particularly so where the metal is depleted uranium, predominantly in ^{238}U form.

Spent Fuel Feed

A variation on the technique, for addressing spent fuel feed materials, is outlined in Figure 3.

Spent fuel, generally comprising of uranium oxide, fission products and plutonium oxides, is introduced at stage 36 and forms the feed to a direct fluorination stage 2. The UF_6 produced and other fluorinated metals are then fed to the separation stage 4.

Given the nature of the feed materials and the desired product forms, impurities are not generally removed from this process route.

As before, the fluorine is recycled back from stage 4 to the direct fluorination stage 2 through stage 6. The products pass on from stage 4 for subsequent handling. The products may form a feed 20 to a subsequent processing stage, or alternatively may form a product form in themselves, stream 38.

A particularly preferred product stream 38 is a mixture of uranium, plutonium and fission products all in metallic form. This product form is intended for long term storage

and represents a considerably improved storage form compared with the material still within a fuel rod or fuel assembly. Not only is the actual form in which the material is present improved, but also the volume of that material is reduced by a factor of 2.5 or so compared with its volume in the actual assembly and additionally the volume of the assembly itself is removed from needing storage. An overall reduction factor of 20 or so in the volume which needs to be stored can be achieved as a result. Another beneficial property of this product form for storage is that uranium metal is a good gamma shield, and as a consequence the material has a self-shielding function against the gamma emissions arising from the fission products contained therein.

Treatment of Enriched Product

As illustrated in Figure 4, a number of enrichment processes, stage 40, including AVLIS, stage 40 provide enriched forms of uranium in metallic or oxide form. This stream 42 frequently contains iron or other impurities which it is desirable to remove before further ~~PROCESSING~~ of the uranium occurs.

In the process route illustrated in Figure 4 the uranium and iron containing stream 42 is fed to a direct fluorination stage 44, the fluorine for which is fed from source stage 46.

It is particularly preferred that the source stage 46 be a separator of the general type outlined in Figure 1 above as separator stage 4, and / or in Figure 2 above as separator stage 32. Once again, it is particularly preferred that the feed material 48 to this stage comprise UF_6 tails and particularly depleted UF_6 . Again, as well as the useful fluorine feed to the fluorination stage 44, a more readily storable and / or handleable product form 50 is produced.

The uranium hexafluoride, iron fluoride and other fluorides produced in the direct fluorination stage can be separated in separator stage 50 based on their differing volatilities. Thus, the relatively volatile UF₆ can be removed as a product stream 52 for subsequent further processing, for instance ~~whereas~~ ^{FABRICATION,} whereas the iron fluoride impurity can be removed as a product stream 54 for subsequent disposal.

Separator Stage

A suitable separator stage, suitable for use in the various embodiments of the present invention is illustrated in Figure 5.

The feed liquor stream 200 passes through a plasma generator 202 which rapidly heats the liquor to around 4000K. The plasma generator 202 may be a microwave or RF type plasma generator and the control of the plasma temperature can readily be provided in this way.

Conducting solenoids in array 206 and 216 produce a high intensity magnetic field whose lines of force are schematically represented 204. The plasma generator and magnetic field are configured such that the components of the feed which are ionised are already within the confines of the magnetic field. The conducting solenoids are set to produce a field intensity in excess of 0.1 Tesla.

As a consequence of the highly elevated temperature of the feed liquor 200 following its passage through the plasma generator 202, the components of the feed liquor 200 break down into their component atoms. This facilitates processing of the feed material according to its individual atomic make up rather than needing an elemental feed or processing the feed only according to differences between the molecules.

At the temperature of the plasma, uranium atoms and other high atomic mass components become charged, U⁺ for instance. The lower atomic mass components, however,

principally fluorine in this case, remains uncharged. Both the ionised and uncharged species are in gaseous form.

By virtue of their charge, the uranium ions are contained by the magnetic field and pass onward through the array of solenoids to form product stream 224. The uncharged nature of the fluorine atoms, however, allows them to move freely and unfettered by the magnetic field, and as a consequence they can be removed as process stream 214 by vacuum pumps or other suitable means. Once clear of the uranium ions, the fluorine can be allowed to fall back in energy and so recombine as F_2 .

As a consequence of this separating stage, therefore, the uranium has been separated from the low atomic weight elements in the feed liquor and the uranium can be sent for subsequent processing or use.

The nature of the selective ionisation which occurs within the separator is important. The ionisation occurs as a result of the overall energy level of the system. Thus, the species which are ionised under the prevailing conditions and the species which are not are determined by the equilibrium state for those species under those conditions. The selective ionisation contained, therefore, is stable and long lasting so allowing the separation to be carried out effectively without pressure of time.

If the energy is introduced into the system such that it is selectively taken up by one species rather than one or another species, then the selective ionisation which is obtained is less useful. In this situation, collisions between the ionised and non-ionised species would result in energy transfer and hence a potential change in the state and / or charge of that species. This places a substantial time pressure on the speed of any separation which must be informed as otherwise the selectivity is lost. Additionally, such ionisations need to be carried out at low densities of

material as otherwise collisions become too dominant for selectivity to occur.

The equilibrium state outlined for the present invention, however, can allow collisions between species to occur without any detriment to the selectivity of the process. As a consequence, a far higher throughput of material is possible.

An alternative separator which can be used is illustrated in Figure 6. Once again, the description of the device will be made in relation to separating uranium from uranium hexafluoride feed, but other applications can readily be made for this apparatus.

The uranium hexafluoride feed liquor is introduced in stream (300) as a vapour. The feed is rapidly converted to a plasma by a radio frequency plasma generator (302). The plasma generator operates at 2KPa in order to ensure essentially equilibrium ionisation levels for the desired components of the feed due to high levels of collisions.

Contact parts within the plasma generator may be formed from ceramic fluorides in order to give the necessary physical properties to withstand the conditions involved. The system may employ copper surface which is cooled by contact with water containing tubes. The water flow is used to lower the temperature of the copper walls and gives rise to condensation of the uranium fluoride forms on the walls. This chemically and thermally insulates the copper. Eventually an equilibrium state develops with a given thickness of the uranium fluoride deposited on the wall. A self-lining effect is thus provided.

The plasma generated exits the generator (302) through nozzle (304) and is contained by magnetic field, schematically illustrated (306). An approximately 30mm radius nozzle is used to maintain the pressure within the plasma generator (304) and to give the desired flow rate.

On leaving the plasma generator and entering zone 1 (308) the plasma will expand giving rise to cooling. However, the work done against the magnetic field by the uranium ions will result in partial re-heating. If appropriate additional energy can be introduced into the plasma during its subsequent progress through the apparatus to maintain the temperature at a level on which the desired components remain ionised. This energy may be provided by radio frequency means. The desired selectivity based on an equilibrium is thus maintained.

The beam of material leaving the plasma generator tends to fan out as the distance from the plasma generator increases.

The barriers (310, 312) defining the various zones take this expansion into account in their selected aperture diameters.

The containing field is approximately 0.1 tesla in strength. Such levels can be provided by conventional electro magnetics although super conducting magnets may be employed. A magnetic field of this strength confines the uranium ions to a radius of 180mm or so following a travel distance of 3m from the nozzle. The zones / stages are each 1m in length. The radius of the expanding beam is approximately proportional to the fourth root of the distance travelled.

Within zone 1 (308) outlets (314) to a vacuum pump, not shown, are provided. These allow first waste streams to be drawn off from the apparatus, the waste streams comprising non-charged material, principally fluorine. Aluminium may be used for the waste stream lines.

The pressure in zone 1 is around 13Pa and during its travel through that zone the fluorine pressure in the material beam reduces substantially to that pressure. The excess fluorine over this is pumped off through outlets (314) using commercially available pumps.

The reduced fluorine content beam then passes into zone 2 (316) through the gap (318) in barrier (310).

The second zone (318) is operated at a lower pressure than the first, approximately 5Pa and once again the fluorine content in the beam reduces towards this pressure as the material passes through the zone.

The beam then passes into zone 3 (320) through gap (322) in barrier (312).

This zone is again operated at a still lower pressure, approximately 2Pa, with the excess fluorine being pumped off through outlets (324).

The significantly depleted fluorine beam then passes on to outlet (326) for subsequent handling.

The ionised, gaseous uranium may be contacted with a grid of some description to discharge the charge and reduce the energy of the uranium to a state in which it is solid or liquid. The introduction of chemical materials to effect a quenching and/or cooling action may be considered. In this regard the use of inert gases to cool the uranium may be preferred so that a chemical combination with the gases does not occur. Metallic uranium arises as a result. The uranium may be cooled sufficiently to provide it as a solid or alternatively may only be partially cooled to leave it in liquid form.

The fluorine remaining in the uranium product stream (326) may be readily volatilised, as a uranium fluoride, from the bulk of the uranium product and recycled. When the uranium is collected as a liquid the separation may conveniently be carried out *in situ*. The volatilised UF will largely be converted to UF₂ which can be recycled.

Provision for collecting fluorine released from the liquid by off gassing may be provided.

For a 12kg uranium per hour feed a 5.7kg/hr fluorine feed arises. Of this fluorine 3.5kg/hr is expected to be pumped off from zone 1; 1.3kg/hr pumped off from zone 2;

0.5kg/hr pumped off from zone 3; and 0.3kg/hr to remain in the uranium product stream (326). Off gassing of the fluorine from this product as UF_4 and / or UF_6 results in a very pure uranium product, ie, a fluorine content in the parts per million range.

Uranium Enrichment Stage

Enrichment of uranium, to increase the portion of ^{235}U , may be effected through a variety of techniques. For instance, the UF_6 produced by the direct fluorination stage 2 of Figure 1 may be removed from the process at stage 10 and be feed to an integral enrichment process and/or an enrichment process at a remote location followin transportation. The enrichment process may be based on gas centrifuging and/or gaseous diffusion separation and/or thermal diffusion based separation.

It is preferred, however, that the uranium exiting separator stage 4 be fed as product stream 20 direct to a subsequent enrichment stage.

ALVIS, atomic vapour laser isotope separation, offers a particularly preferable form of enrichment. An AVLIS type enricher rendered suitable for use in the present invention is illustrated in Figure 7. The enricher 70 consists of a vessel 72 into which a feed stream is introduced along passage 74. The vessel 72 is evacuated using pump 76 to a low pressure, generally less than 10^{-6} torr.

Where the enricher 70 follows a separator 4, as illustrated in Figure 1 or 3, then the feed is generally uranium metal in atomic vapour form.

Where the enricher 70 is followed by a direct fluorination stage 44, as illustrated in Figure 4, then the feed may be atomic vapour from a previous stage (such as a separator of the above mentioned type) or the enricher may be provided with capability to convert the feed into an atomic vapour form. This facility may be provided (not shown) by inductive heating and/or resistive heating and/or electron beam application.

Once introduced into the vessel 72 the feed stream 78 contacts laser radiation 80 introduced from a laser through window 82 in the vessel 72. The frequency or frequencies of the radiation are carefully selected such that they cause photoionisation of one set of isotopes, but not of the other set of isotopes. In the case of uranium, the frequency is generally selected to excite ^{235}U , but not ^{238}U .

Once converted to an ionised form, the ions are electrostatically attracted to collection plates 84. The enriched material collected can be periodically or continuously removed from the collector plates 84. The non-ionised forms are not attracted to the charged plates 84 and hence continue to separate collector 86.

The enriched material collected at plates 84 normally contains other components too, such as iron and iron oxides and these are removed based on volatility as discussed above in relation to Figure 4. A similar separation technique may be used to remove impurities from the depleted material collected by collector 86.

As an alternative to AVLIS, particularly with regard to the process set out in Figure 4, the enrichment stage could be effected by MLIS, molecular laser isotope separation. In MLIS molecules incorporating the different isotopes are provided in gaseous form and selectively photoionised. A separation based on charged and non-charged molecules can then be made in a similar way to that outlined for AVLIS above.

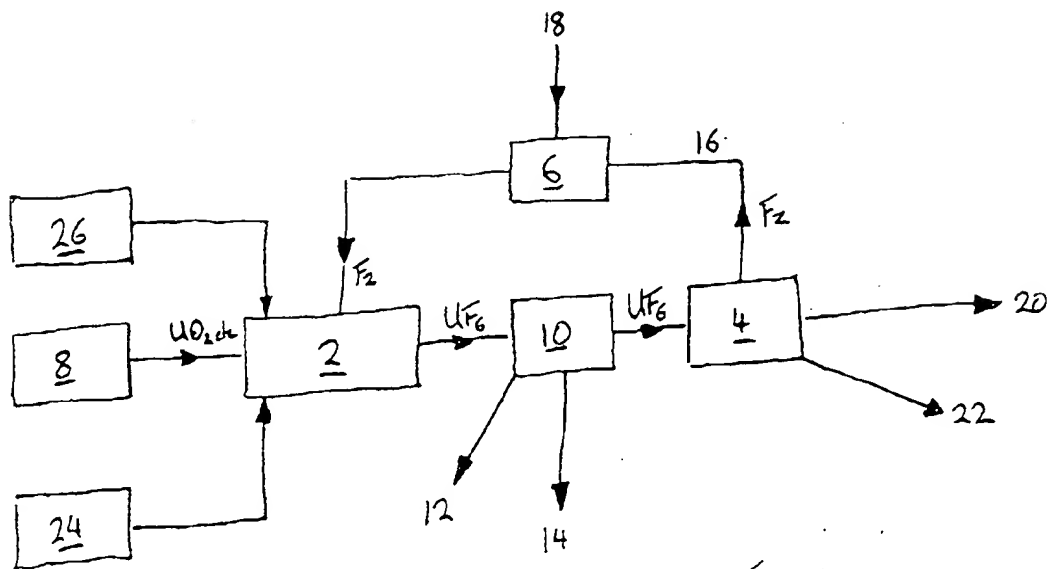


Fig 1

Fig 2

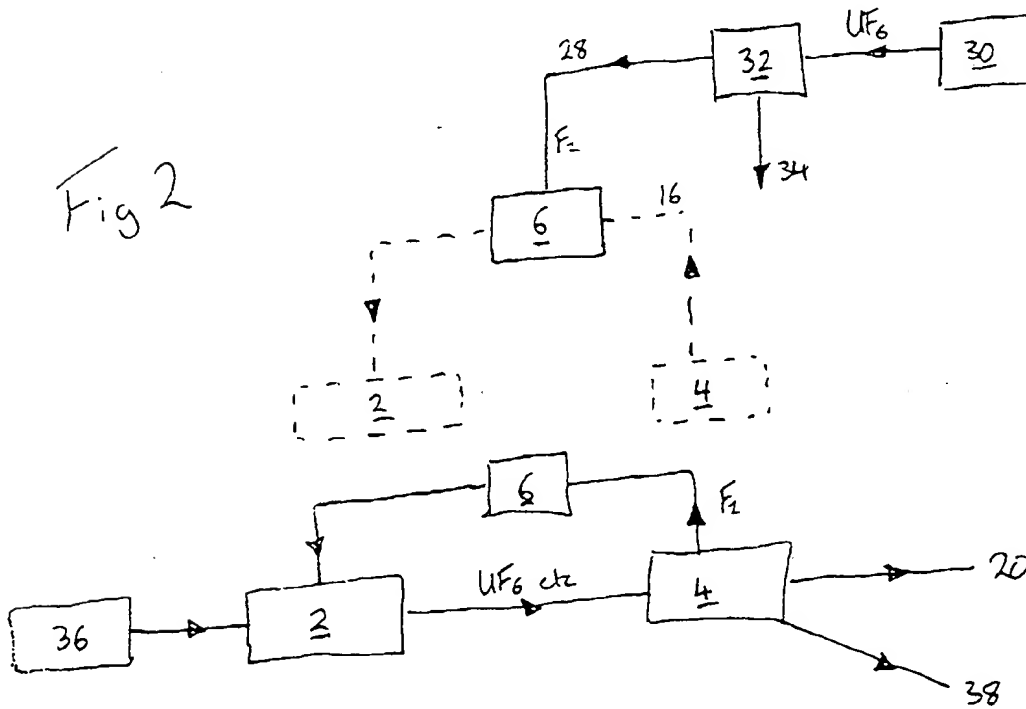
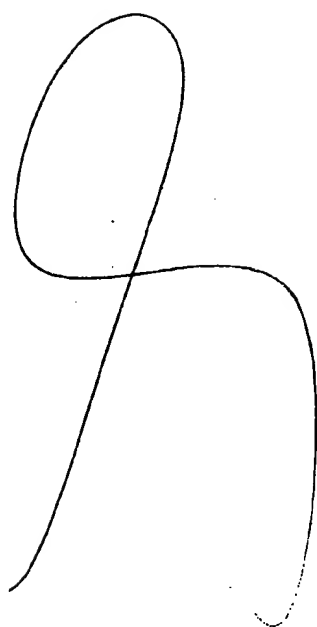


Fig 3



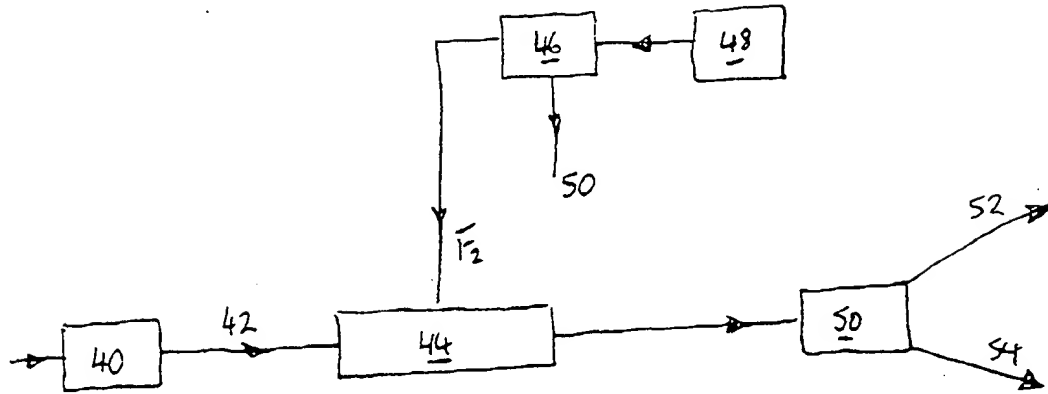


Fig 4.

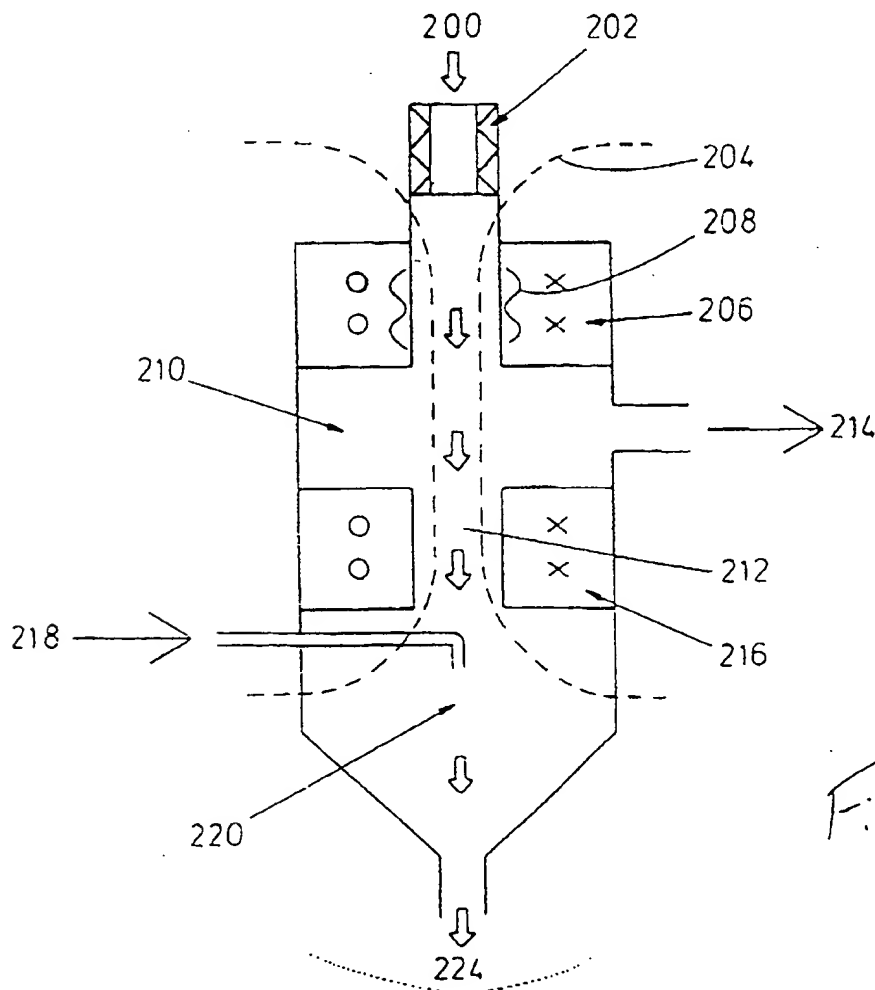


Fig 5

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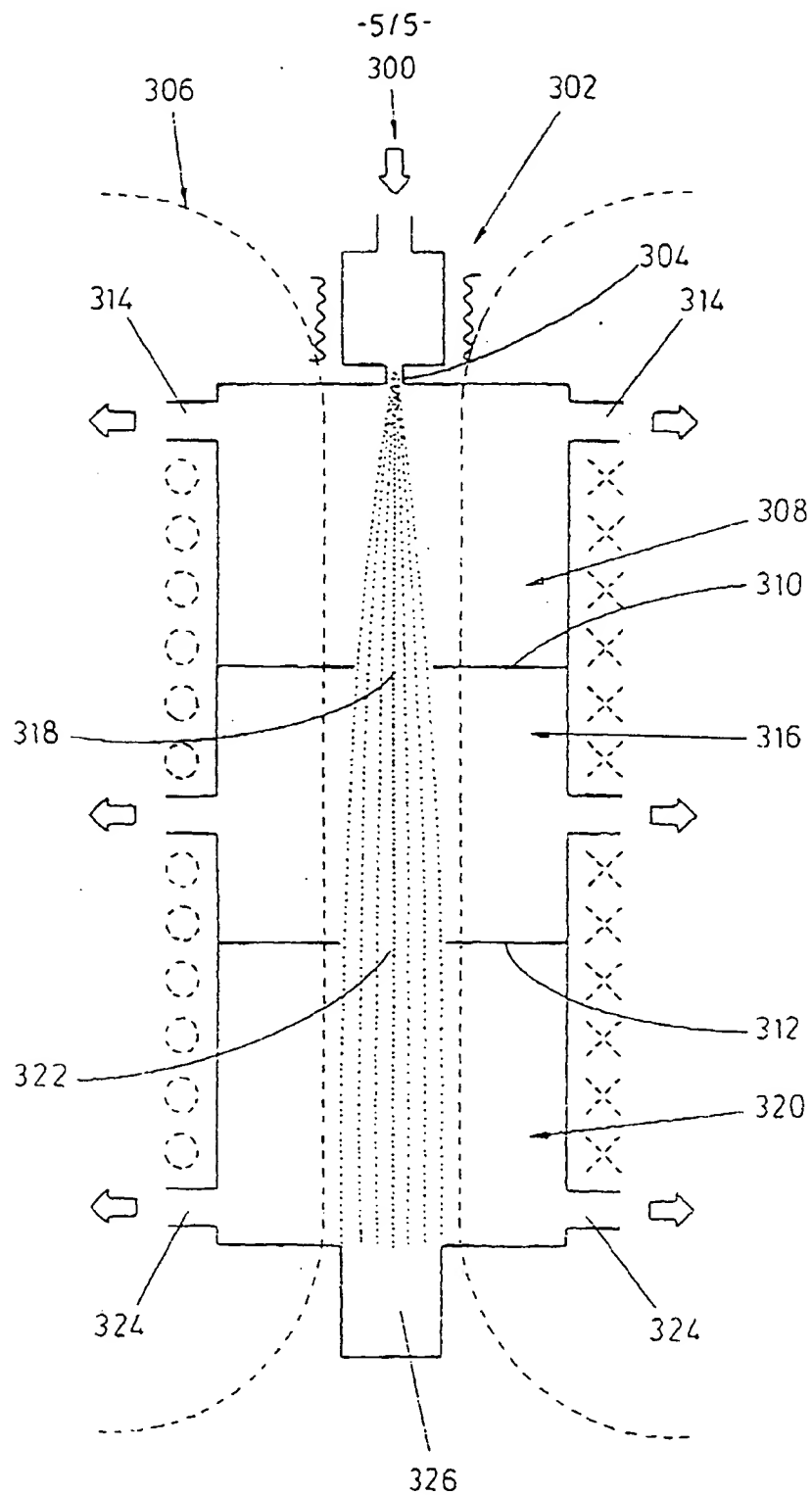


FIG. 6

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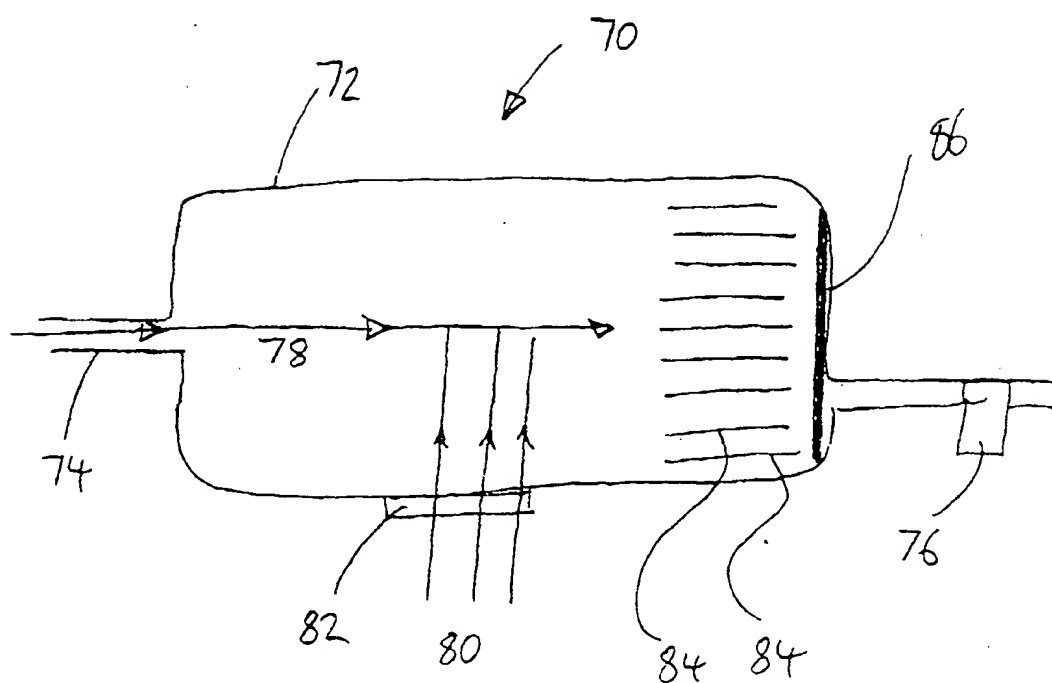


Fig 7

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